

# NITROGEN REMOVAL

GRANT WEAVER, PE & WWTP OPERATOR  
PRESIDENT  
THE WATER PLANET COMPANY



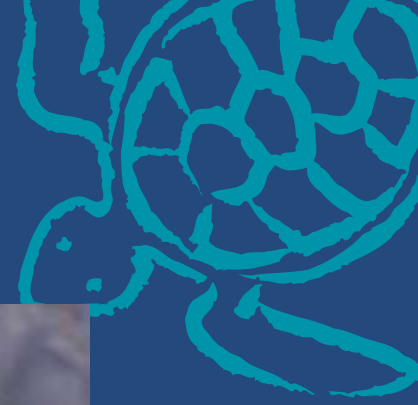
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# *Creating Optimal Habitats*



## *Creating Optimal Habitats*



# THE SCIENTIFIC METHOD

? **PURPOSE** ?  
WHAT DO I WANT TO LEARN?

**Research**

Find out as much about your topic as you can.



**HYPOTHESIS**

Predict what the answer to the problem is.

**EXPERIMENT**

Design a test to confirm or disprove your hypothesis.



**Analysis**

Record what happened during the experiment.

**Conclusion**

Was my hypothesis correct?



*Wastewater Science*  
*Alkalinity and pH*

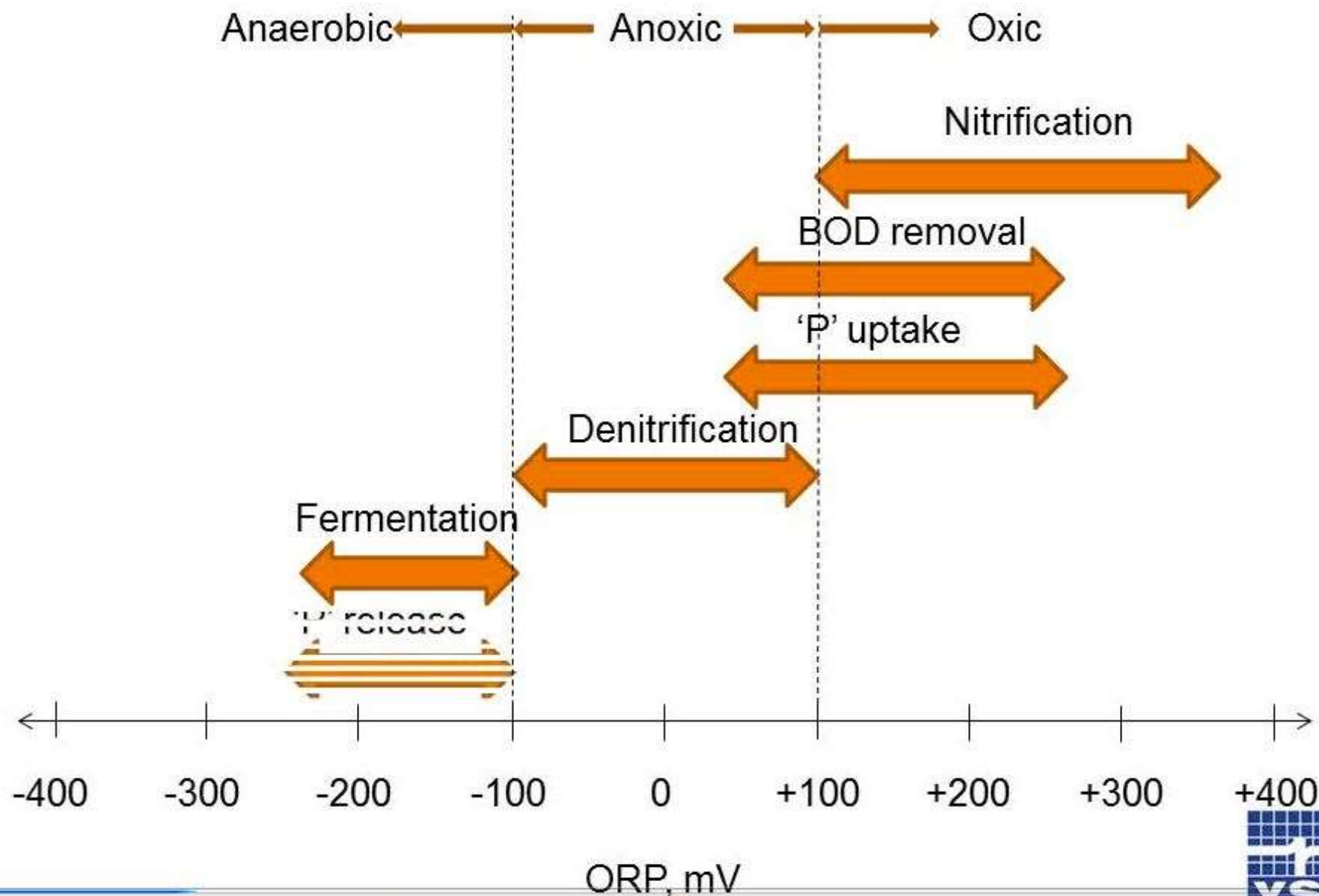


# Wastewater Science

## DO and ORP



# What does ORP tell us about our process?



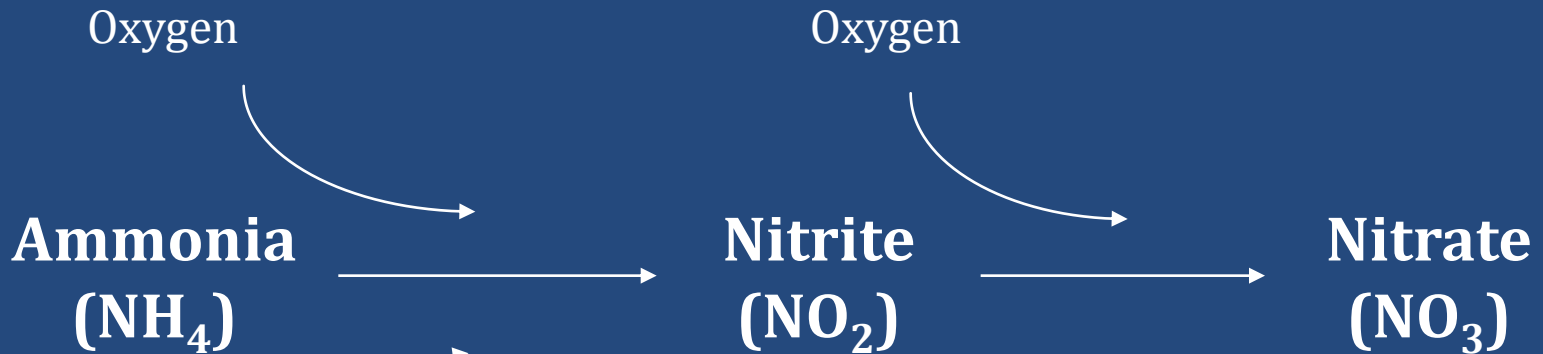




*Biological Nitrogen Removal:  
Convert liquid to gas ...*



# Ammonia Removal



**Nitrification Habitat:**  
High DO / +ORP  
Low BOD  
High MLSS/MCRT  
High HRT

Consumes oxygen  
Consumes alkalinity: lowers pH

## *Nitrification:*

*Ammonia ( $\text{NH}_4$ ) is converted to Nitrate ( $\text{NO}_3$ )*

### Oxygen Rich Habitat

MLSS\* of 2500+ mg/L (High Sludge Age / MCRT / low F:M)

ORP\* of +100 to +150 mV (High DO)

Time\* (high HRT ... 24 hr, 12 hr, 6 hr, 4 hr)

Low BOD

Consumes Oxygen

Adds acid - Consumes 7 mg/L alkalinity per mg/L of  $\text{NH}_4 \rightarrow \text{NO}_3$

\*Approximate, each facility is different.



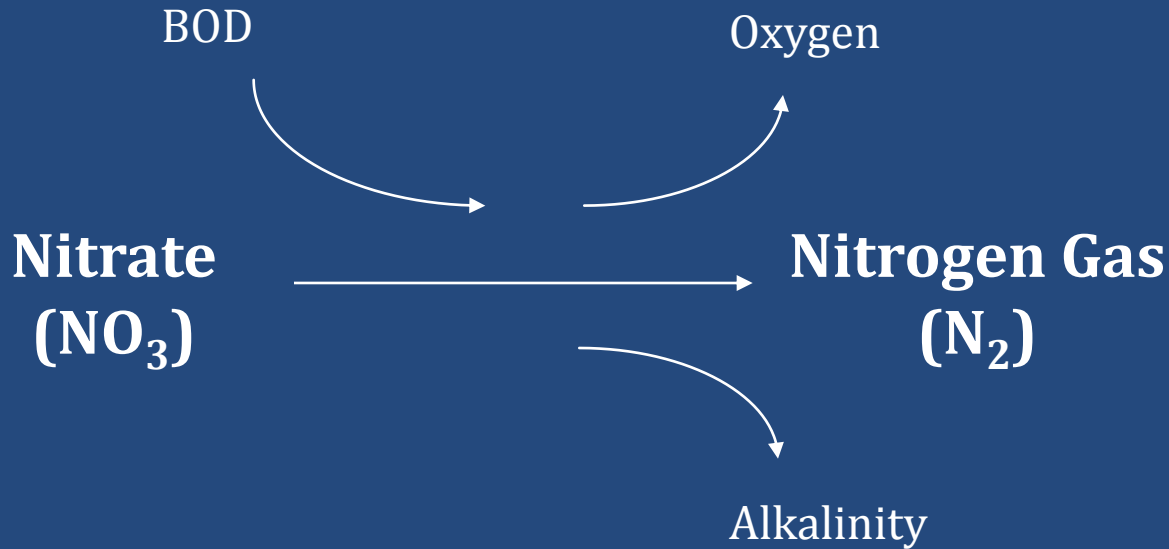
*Biological Nitrogen Removal:*

*Next,*

*The Nitrate ( $\text{NO}_3$ ) created during Nitrification ...  
is converted to Nitrogen Gas ( $\text{N}_2$ )*



## *Nitrate Removal*



### Denitrification Habitat:

Low DO / -ORP  
High BOD

Adds DO

Gives back ½ the alkalinity: beneficially raises pH



## *Denitrification:*

*Nitrate ( $\text{NO}_3$ ) is converted to Nitrogen Gas ( $\text{N}_2$ )*

### Oxygen Poor Habitat

ORP\* of -100 mV or less (DO < 0.3 mg/L)

Surplus BOD\* (100-250 mg/L: 5-10 times as much as  $\text{NO}_3$ )

Retention Time\* of 45-90 minutes

Gives back Oxygen

Gives back Alkalinity (3.5 mg/L per mg/L of  $\text{NO}_3 \rightarrow \text{N}_2$ )

\*Approximate, each facility is different.





## *Nitrogen Terms for Operators*

**organic-Nitrogen** (org-N or  $N_{\text{org}}$ )

**Ammonia** ( $\text{NH}_3$ )

**Ammonium** ( $\text{NH}_4$  or  $\text{NH}_4^+$ )

**TKN** (Total Kjeldahl Nitrogen)

= organic-Nitrogen + Ammonia

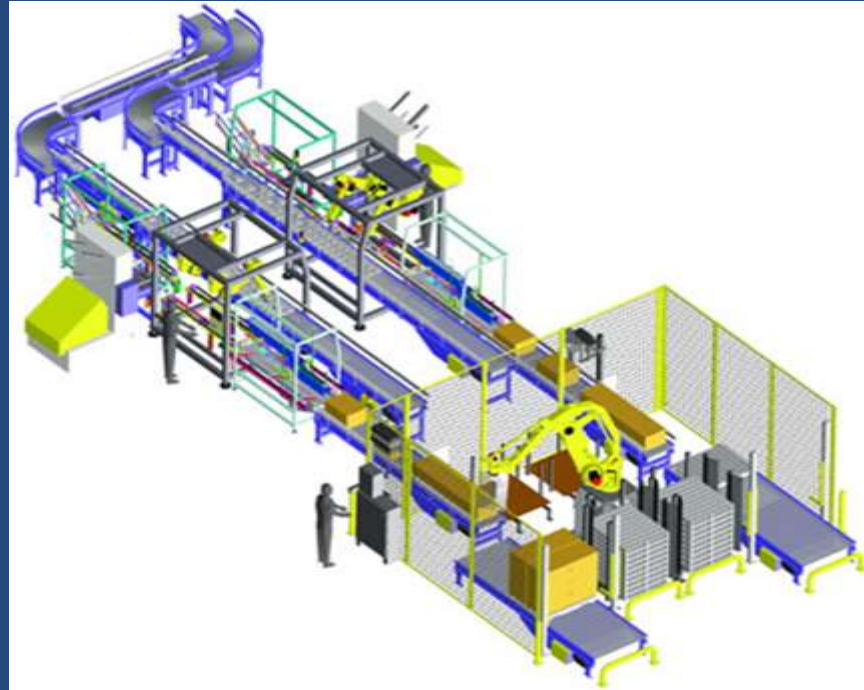
**Nitrate** ( $\text{NO}_3$  or  $\text{NO}_3^-$ )

**Nitrite** ( $\text{NO}_2$  or  $\text{NO}_2^-$ )

**total Nitrogen** (total-N, N, TN, tN, or  $N_{\text{total}}$ )

= TKN + Nitrate + Nitrite

# *Technology!*

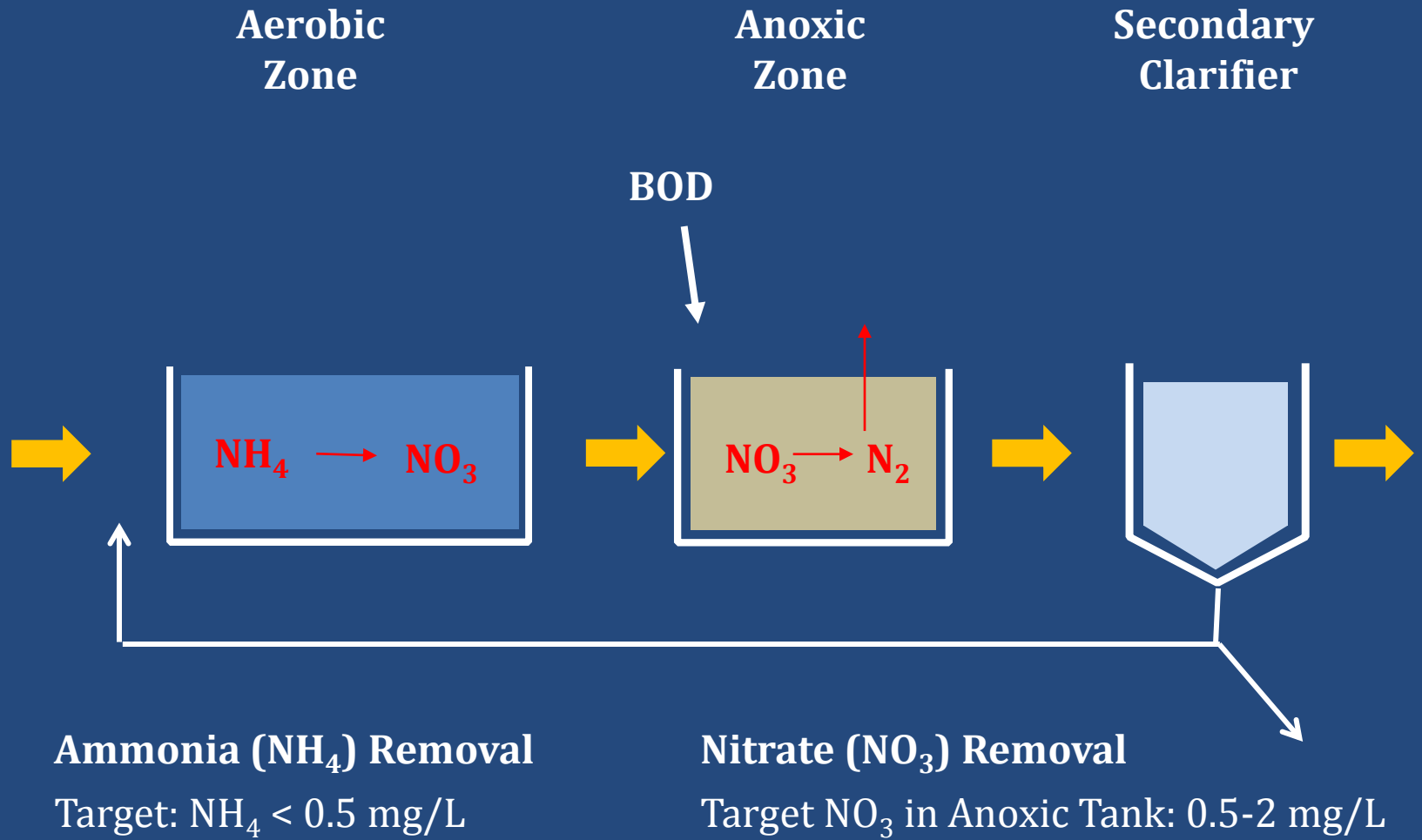




*Post Denitrification*



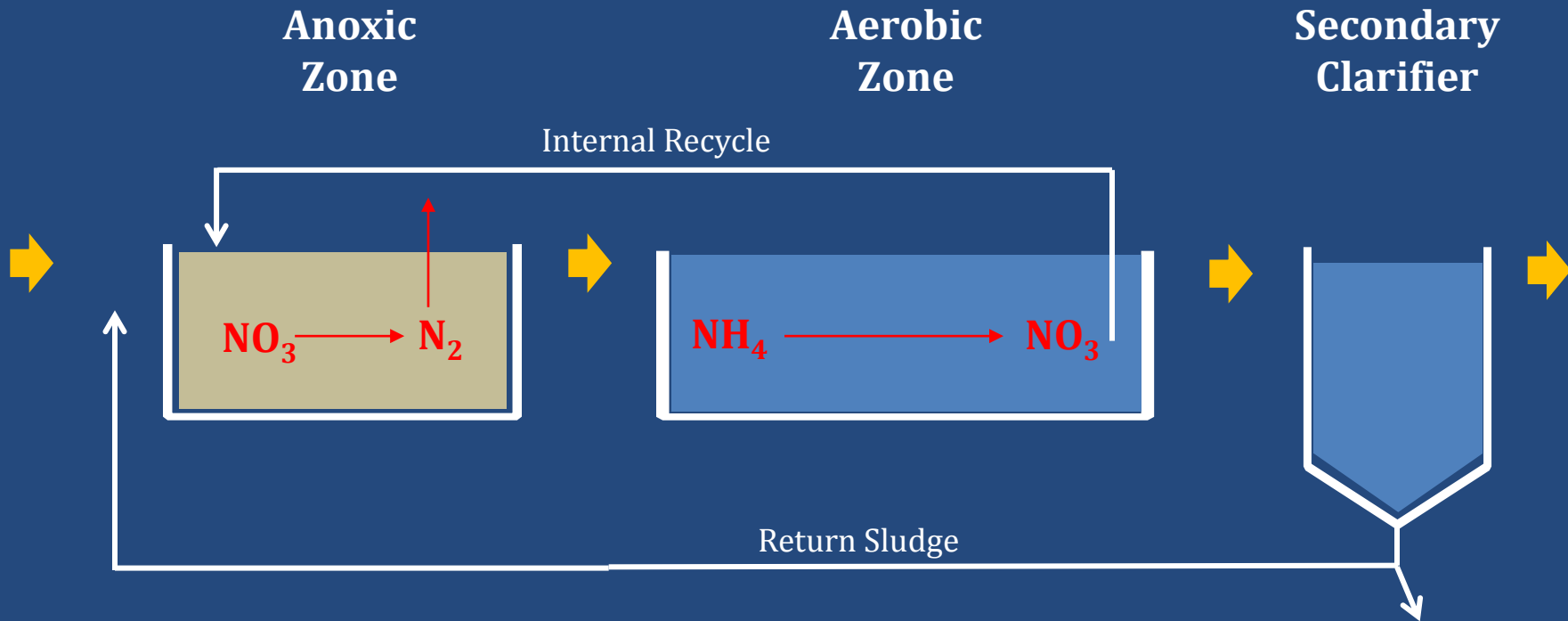
# Post-Anoxic Denitrification



*MLE (Modified Ludzack-Ettinger) Process*



# MLE (Modified Ludzack-Ettinger) Process



## MLE Process Control:

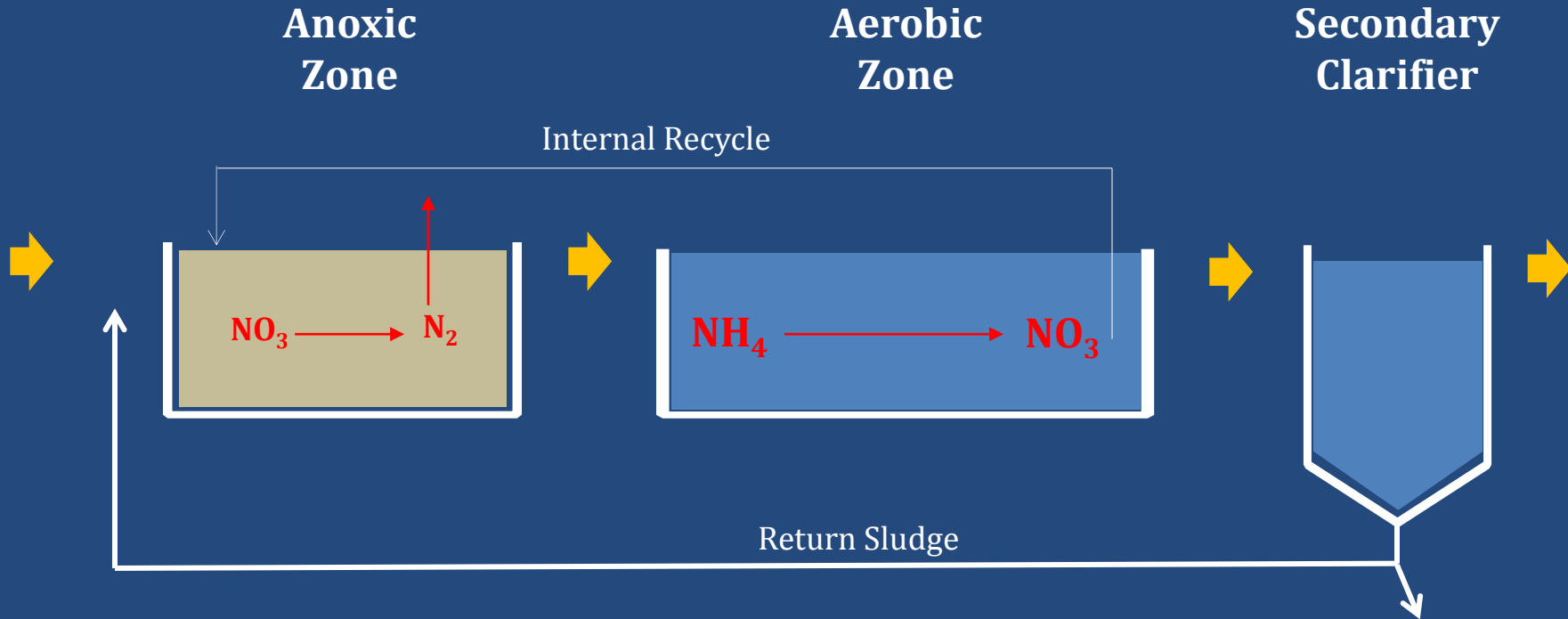
Proper Internal Recycle Rate; not too much / not too little.

ORP of +100 mV in Aerobic Zone for Ammonia ( $\text{NH}_4$ ) Removal.

ORP of -75 to -150 mV in Anoxic Zone for Nitrate ( $\text{NO}_3$ ) Removal.

Enough BOD to support Nitrate ( $\text{NO}_3$ ) Removal.

# MLE with not enough Internal Recycle



## Ammonia ( $\text{NH}_4$ ) Removal

Excellent Aerobic Habitat: ORP +150 mV

$\text{NH}_4 < 0.5 \text{ mg/L}$

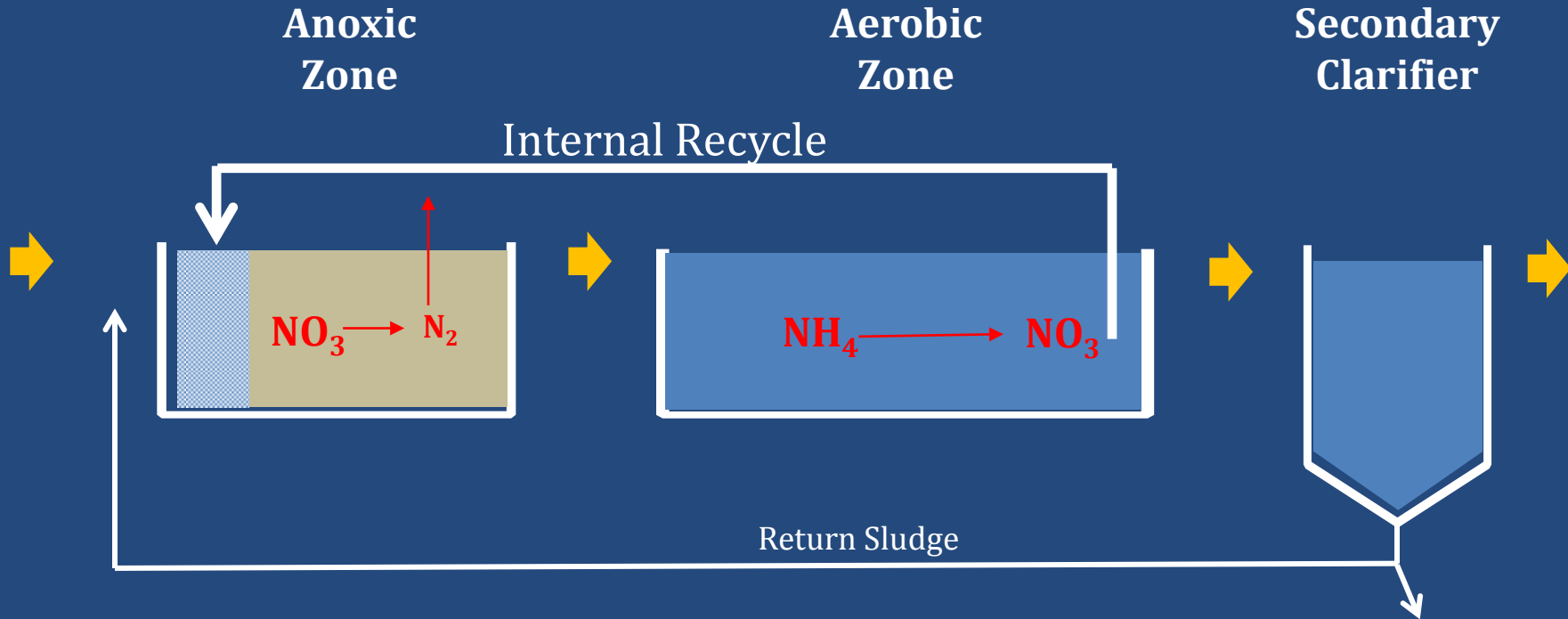
## Nitrate ( $\text{NO}_3$ ) Removal

Great Anoxic Habitat: ORP -150 mV or lower

$\text{NO}_3 > 4 \text{ mg/L}$  because too little  $\text{NO}_3$  is returned to Anoxic Zone



# MLE with too much Internal Recycle



## Ammonia ( $\text{NH}_4$ ) Removal

Good Aerobic Habitat: ORP +100 mV

$\text{NH}_4 < 0.5 \text{ mg/L}$

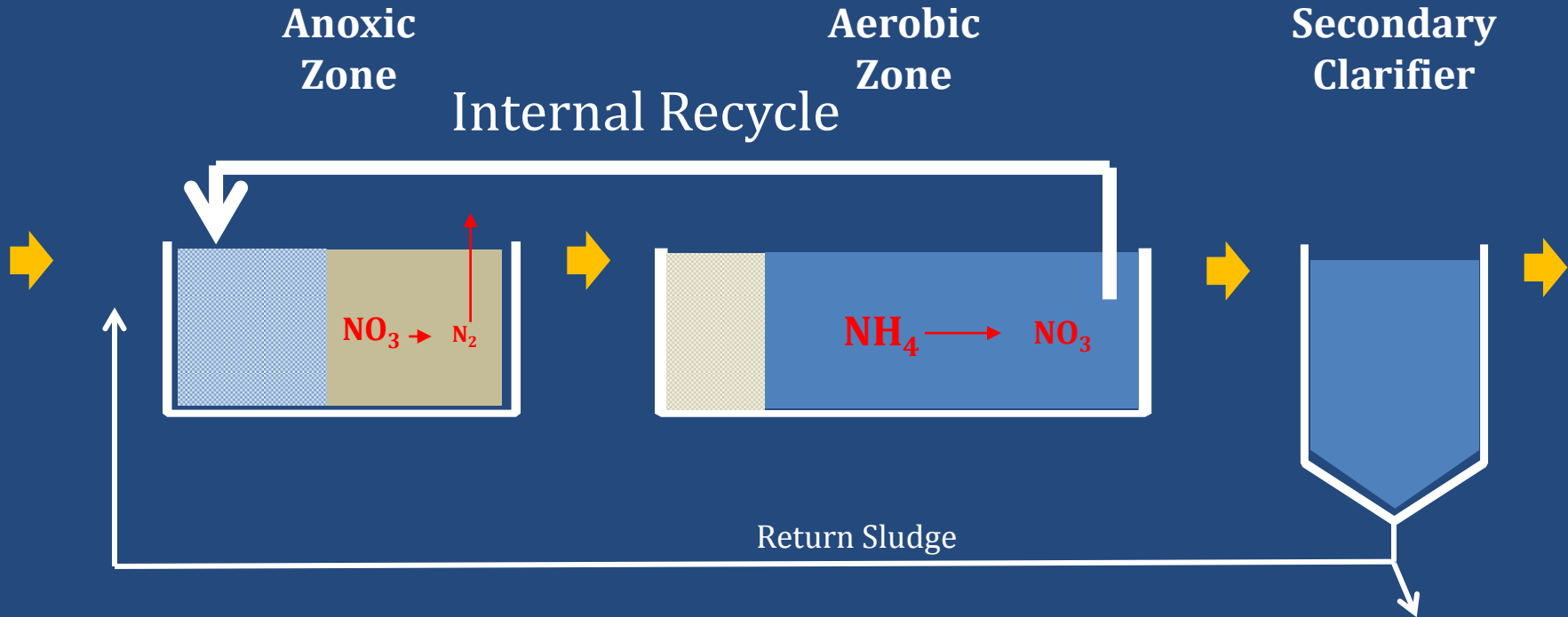
## Nitrate ( $\text{NO}_3$ ) Removal

Stressed Anoxic Habitat: ORP 0 to -100 mV

$\text{NO}_3 > 4 \text{ mg/L}$ : bacteria will not convert Ammonia ( $\text{NH}_4$ ) to Nitrate ( $\text{NO}_3$ )



# MLE with way too much Internal Recycle



## Ammonia ( $\text{NH}_4$ ) Removal

Poor Aerobic Habitat: ORP +50 mV

$\text{NH}_4 > 0.5 \text{ mg/L}$

## Nitrate ( $\text{NO}_3$ ) Removal

Poor Anoxic Habitat: ORP 0 mV or higher

$\text{NO}_3 > 4 \text{ mg/L}$

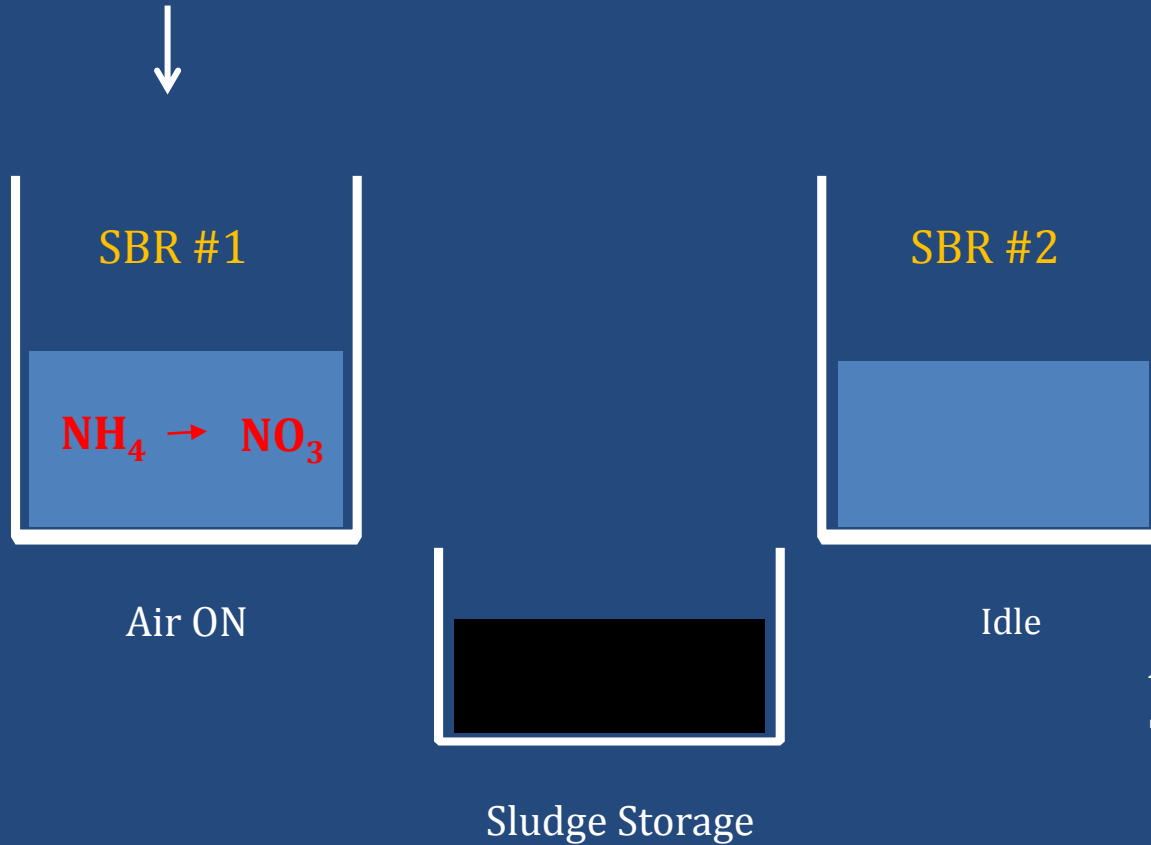


*Sequencing Batch Reactor  
SBR*





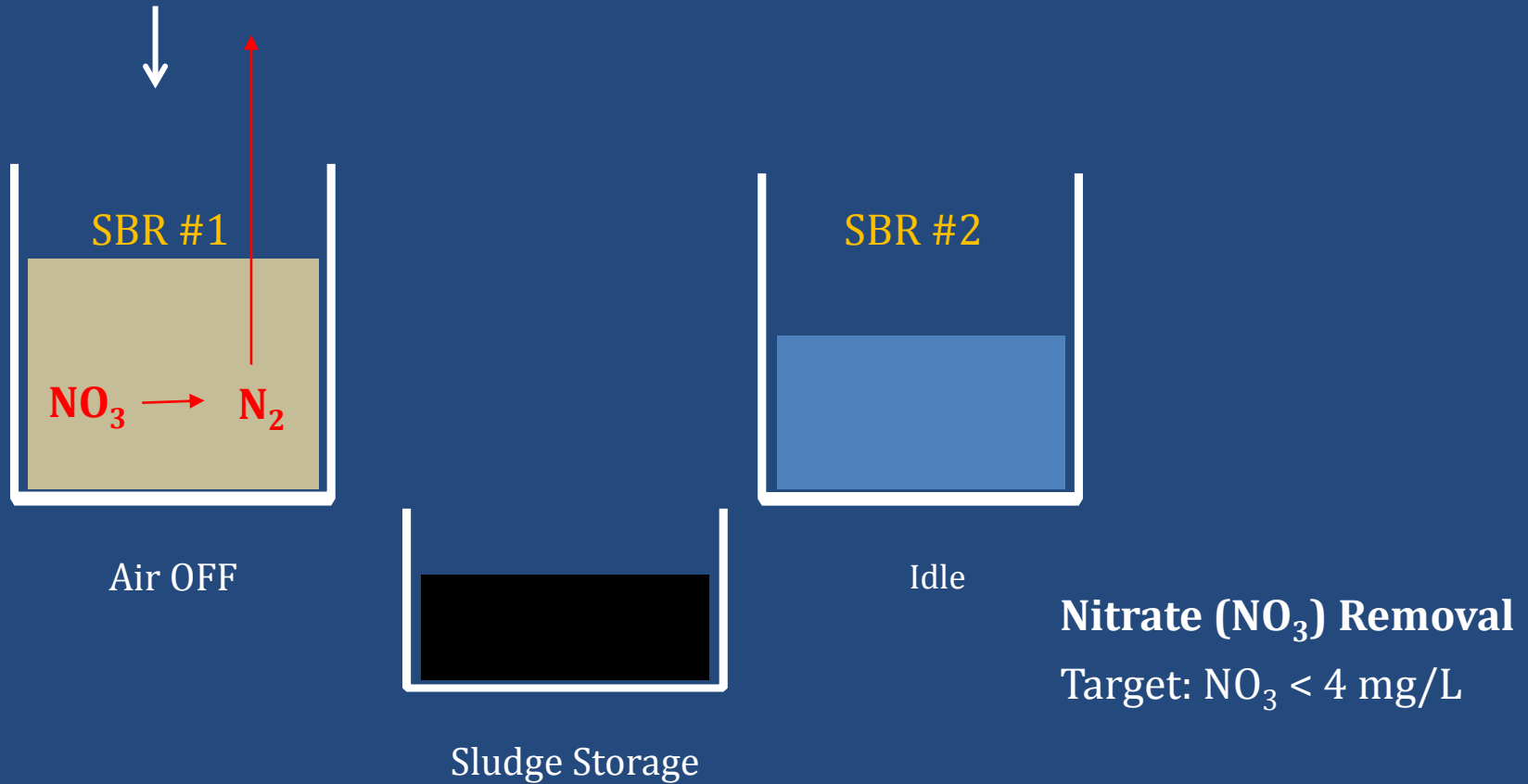
# Sequencing Batch Reactor (SBR) Ammonia ( $\text{NH}_4$ ) Removal: Nitrification



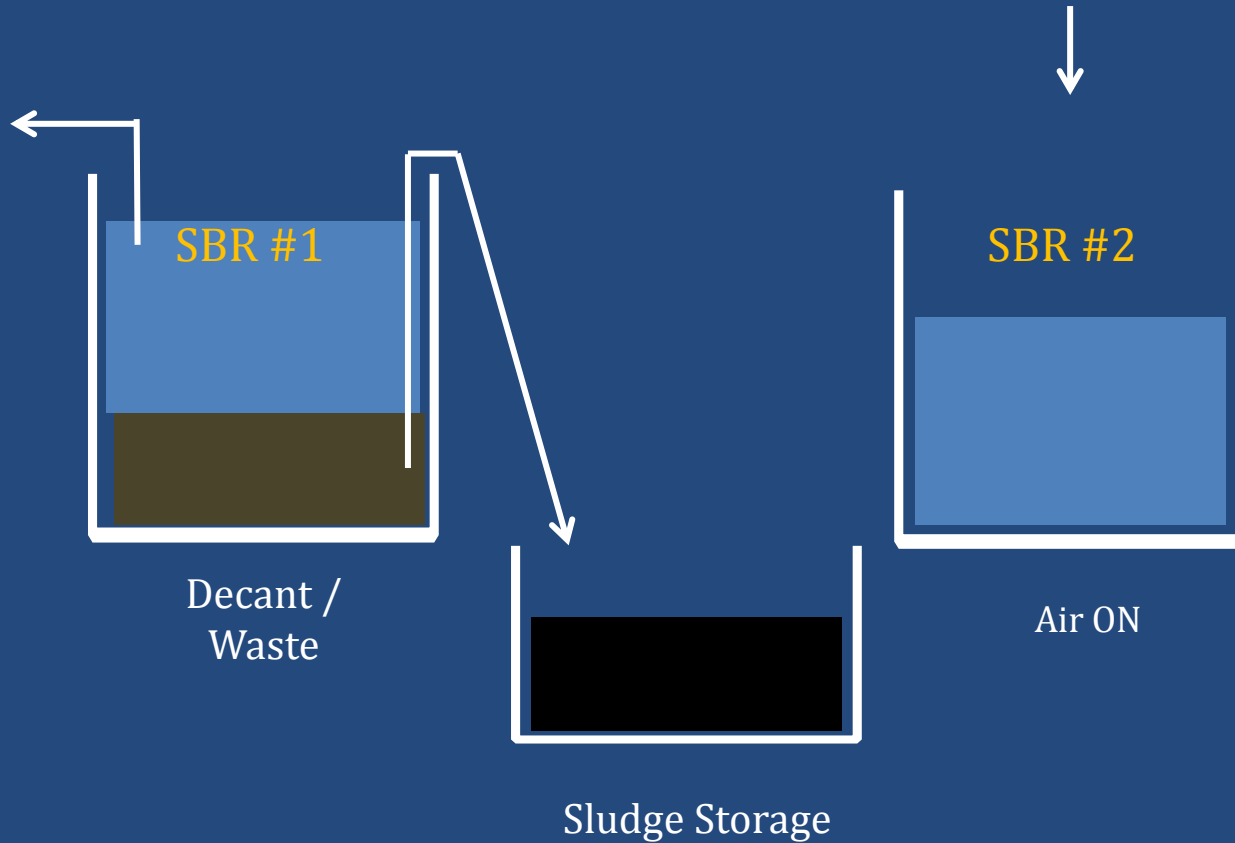
**Ammonia ( $\text{NH}_4$ ) Removal**

Target:  $\text{NH}_4 < 0.5 \text{ mg/L}$

# Sequencing Batch Reactor (SBR) Nitrate ( $\text{NO}_3$ ) Removal: Denitrification



# Sequencing Batch Reactor (SBR) Settle, Decant & Waste Sludge



SBR Process Control:

Establish cycle times that are long enough to provide optimal habitats.

And, short enough to allow all of the flow to be nitrified and denitrified.

## *Optimizing SBR cycle time*

### Too short

Will not reach +100 mV for Ammonia ( $\text{NH}_4$ ) Removal.

Will not reach -100 mV for Nitrate ( $\text{NO}_3$ ) Removal.

Note: Temperature and BOD affect Air OFF cycle.

### Too long

Wastewater will pass through tank before all Ammonia ( $\text{NH}_4$ ) converted to Nitrate ( $\text{NO}_3$ ).

And, before all Nitrate ( $\text{NO}_3$ ) is converted to Nitrogen Gas ( $\text{N}_2$ ).

### Just right

Good habitats ...

ORP of +100 mV for 60 minutes

And, ORP of -100 mV for 30 minutes.

Bonus: Changing conditions will serve as a selector.



*Oxidation Ditch  
4-Stage Bardenpho*



# Oxidation Ditch – 4-Stage Bardenpho

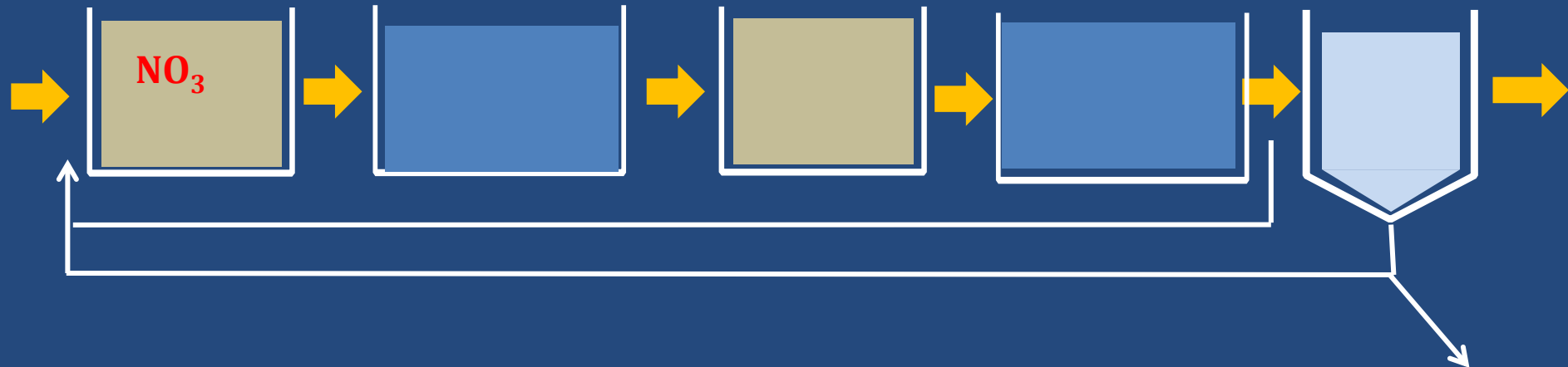
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

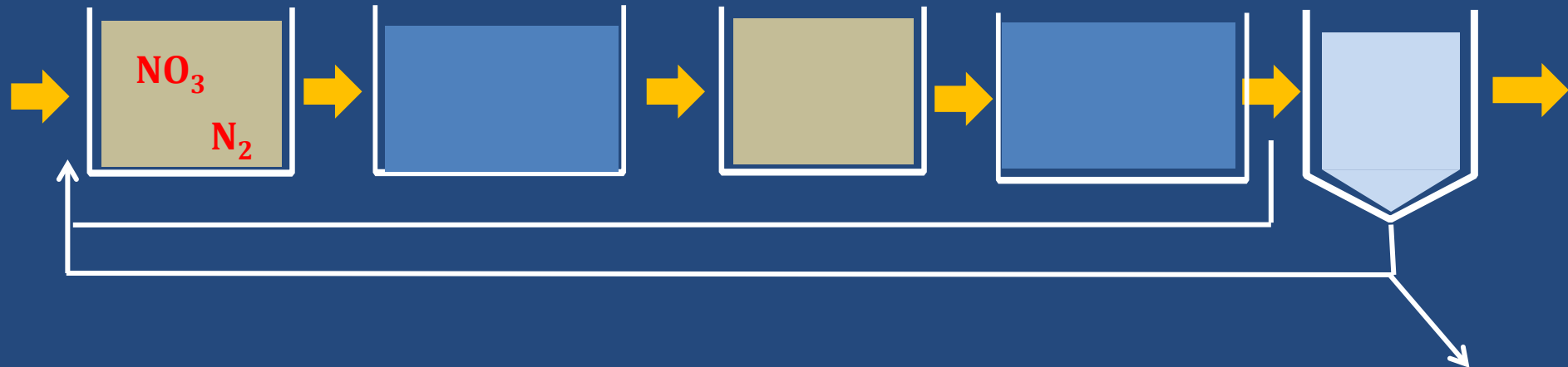
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

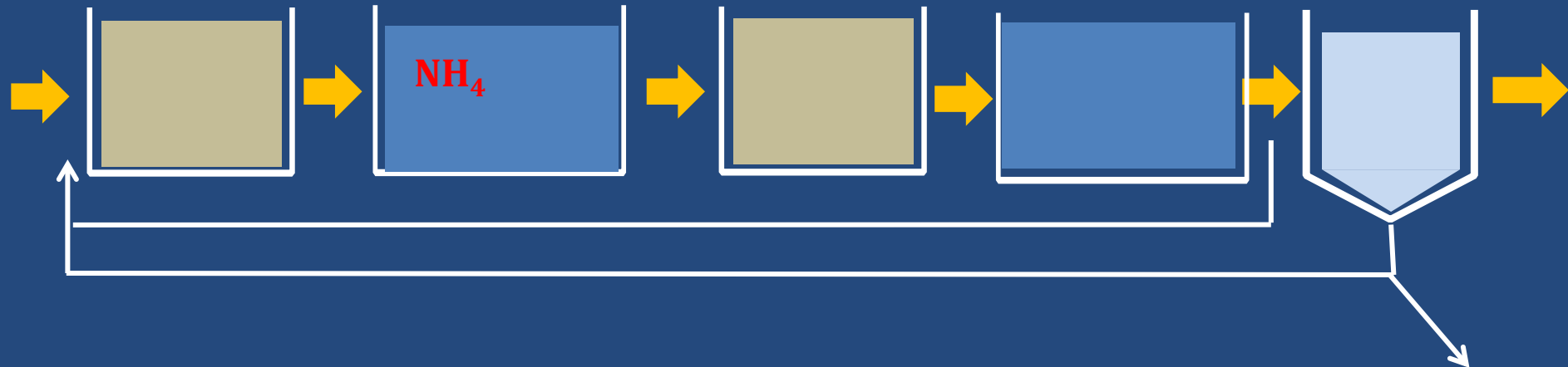
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier





# Oxidation Ditch – 4-Stage Bardenpho

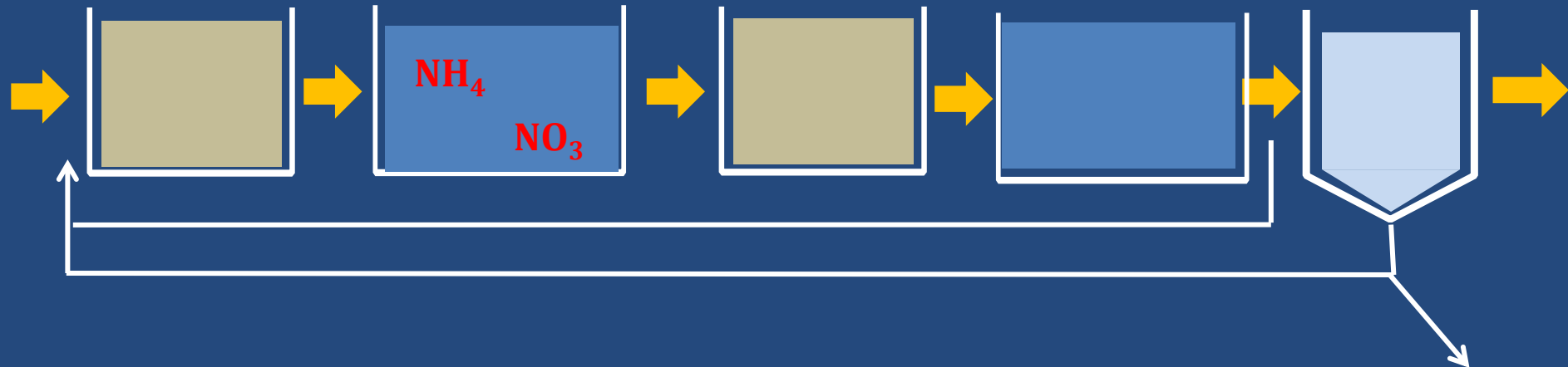
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

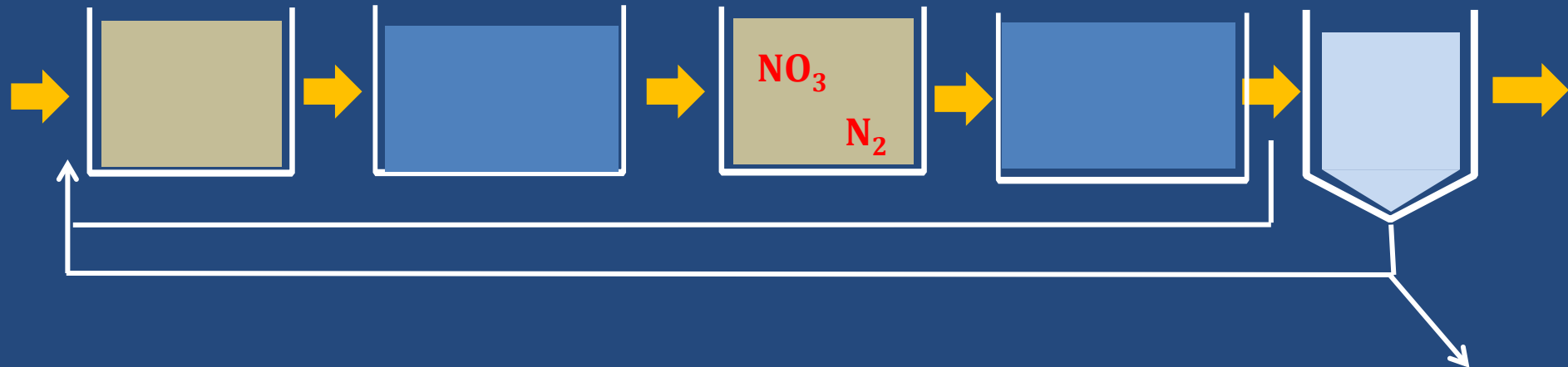
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

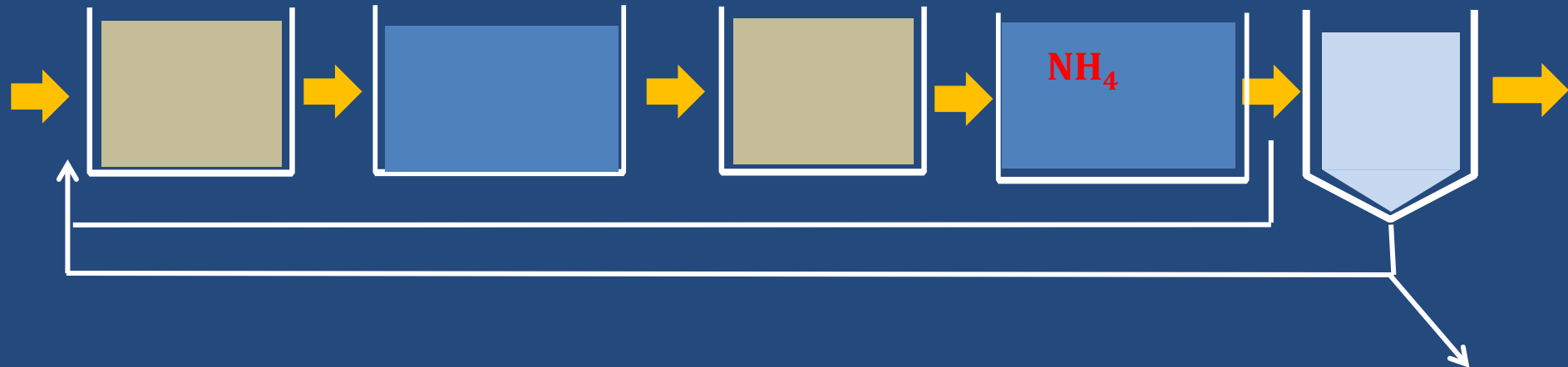
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

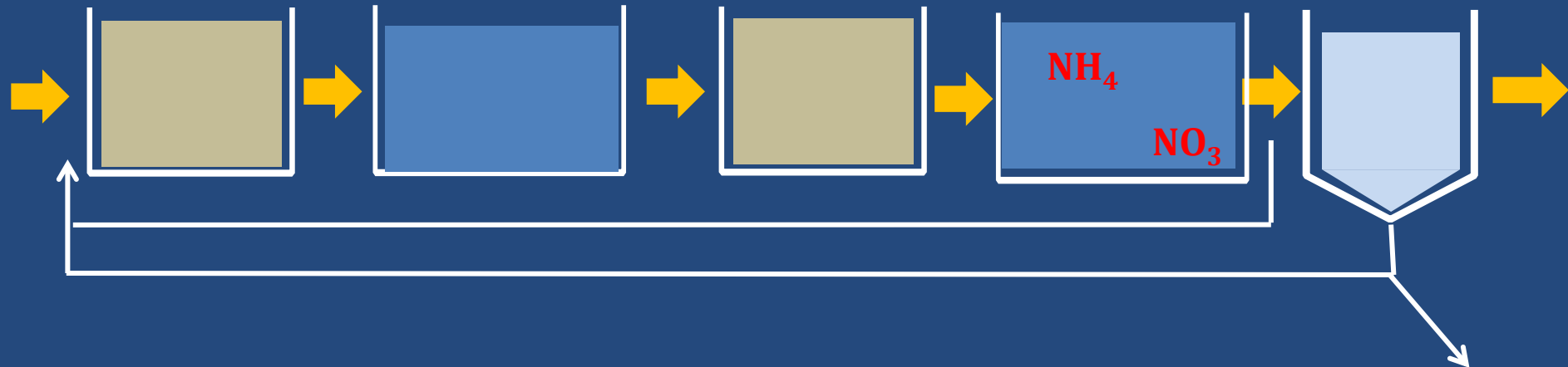
Anoxic  
Zone

Aerobic  
Zone

Anoxic  
Zone

Aerobic  
Zone

Secondary  
Clarifier



# Oxidation Ditch – 4-Stage Bardenpho

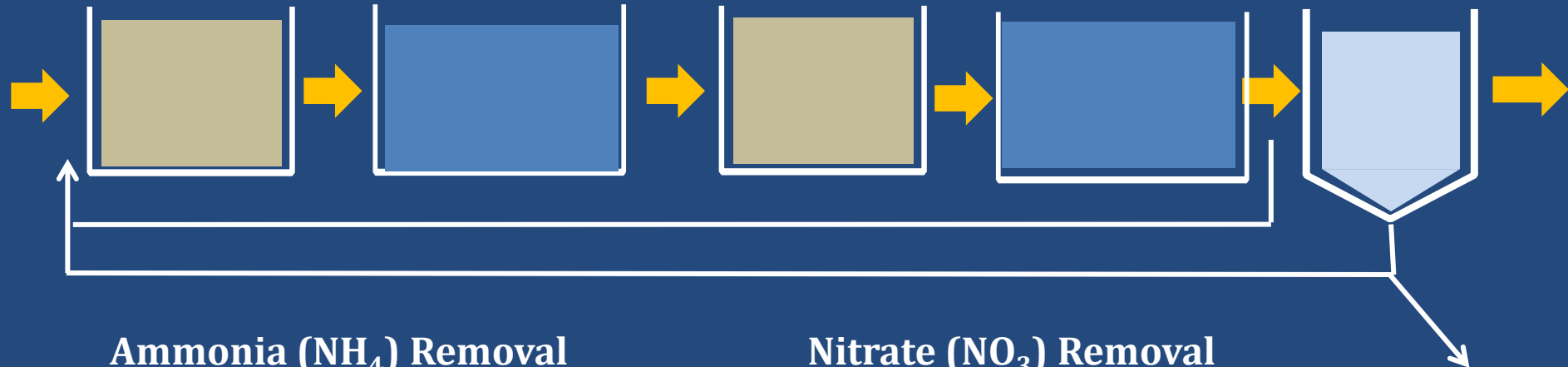
**Anoxic  
Zone**

**Aerobic  
Zone**

**Anoxic  
Zone**

**Aerobic  
Zone**

**Secondary  
Clarifier**



**Ammonia (NH<sub>4</sub>) Removal**

Target: NH<sub>4</sub> < 0.5 mg/L

**Nitrate (NO<sub>3</sub>) Removal**

Target: NO<sub>3</sub> of 1-4 mg/L

**BACKGROUND  
INFORMATION**



*Experimenting with YOUR plant:  
Finding the “Right” Process Control Strategy*



*... and, Optimizing Nitrogen Removal*



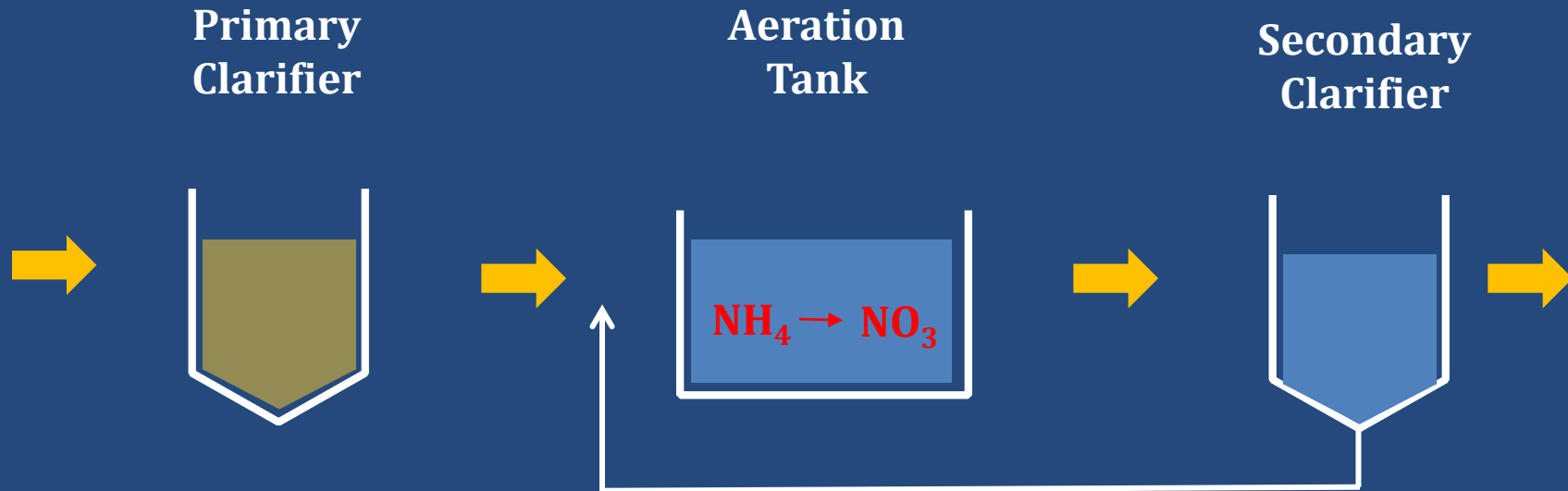
# Step 1

*Optimize Ammonia ( $\text{NH}_4$ ) Removal*





# Conventional Activated Sludge Plant



## Ammonia ( $\text{NH}_4$ ) Removal

**Target: less than 0.5 mg/L**

Raise mixed liquor

... the higher the better for N-Removal.

Keep ORP at +100 mV (or higher) by adjusting DO settings until ...

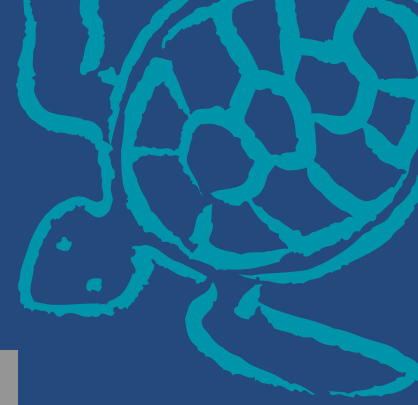
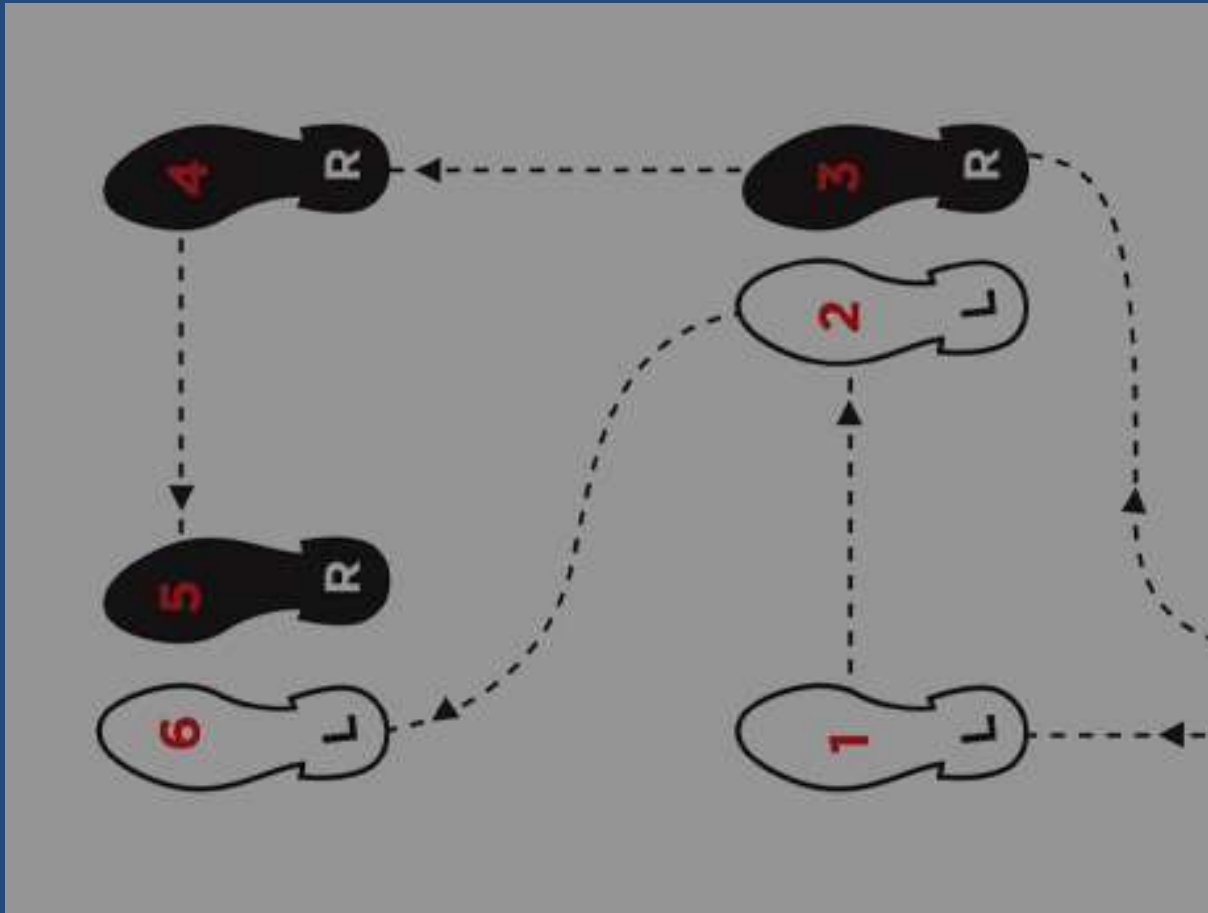
... enough DO & ORP to reduce  $\text{NH}_4$  to 0.5 mg/L ...

... but not so much as to move too much DO into Anoxic or waste electricity.

Warning: pH and Nitrite ( $\text{NO}_2$ )



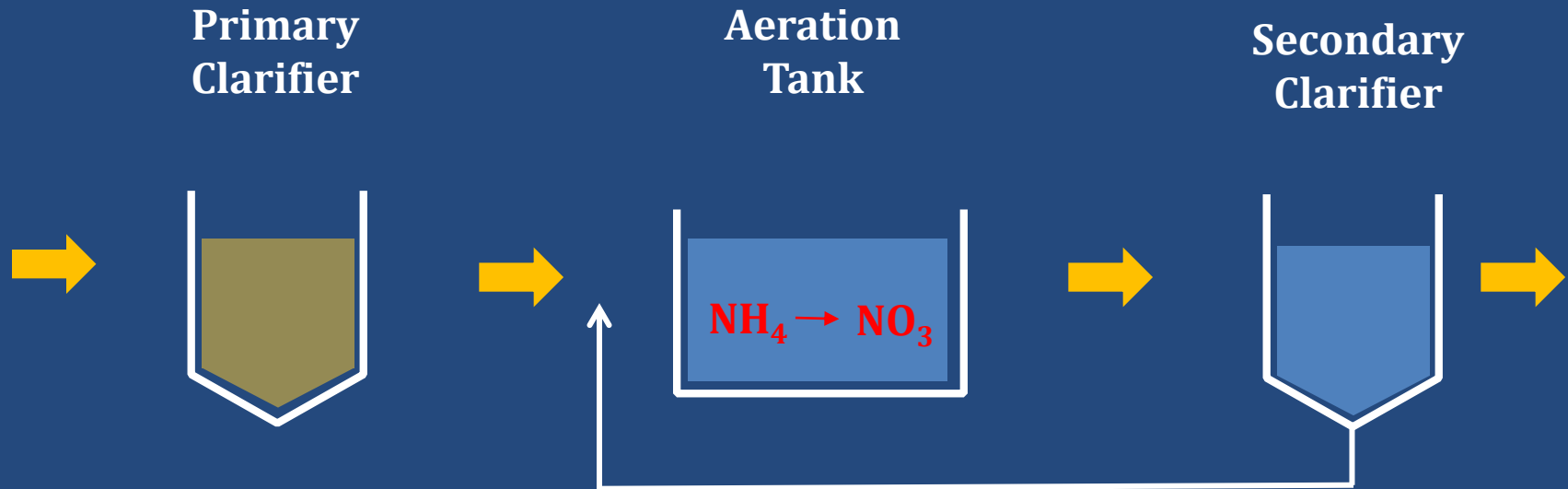
## Step 2: Optimize Nitrate ( $\text{NO}_3$ ) Removal



*Operate Aeration Tank as SBR*



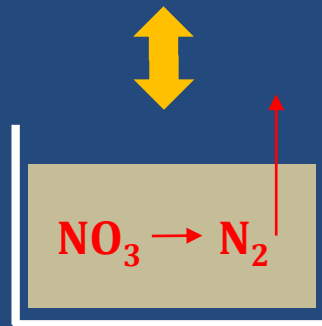
# Conventional Activated Sludge operated as SBR



## Maintain Ammonia ( $\text{NH}_4$ ) Removal

Target:  $\text{NH}_4 < 0.5 \text{ mg/L}$   
ORP: +100 mV long enough  
(60 minutes)

Cycle air ON to remove  $\text{NH}_4$  & OFF to remove  $\text{NO}_3$   
Use ORP to adjust AirON/AirOFF times



## Nitrate ( $\text{NO}_3$ ) Removal

Target:  $\text{NO}_3 < 4 \text{ mg/L}$   
ORP: -100 mV long enough (30 minutes)

If habitats are good and  $\text{NO}_3$  remains high, likely not enough BOD.

Search for additional BOD.

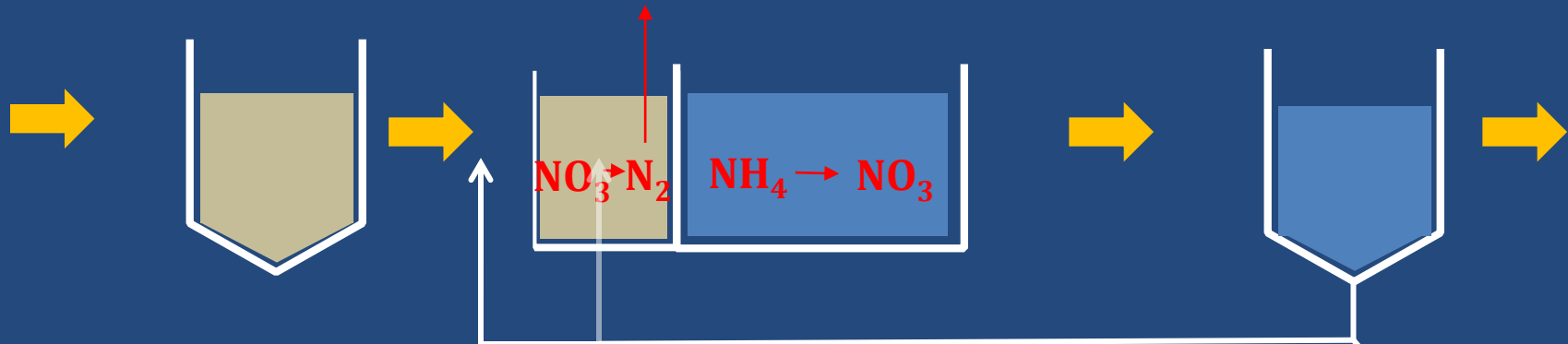
*Operate Aeration Tank as MLE*



## Primary Clarifier

## Aeration Tank

## Secondary Clarifier



### Maintain Ammonia ( $\text{NH}_4$ ) Removal

Target:  $\text{NH}_4 < 0.5 \text{ mg/L}$   
ORP: +100 mV

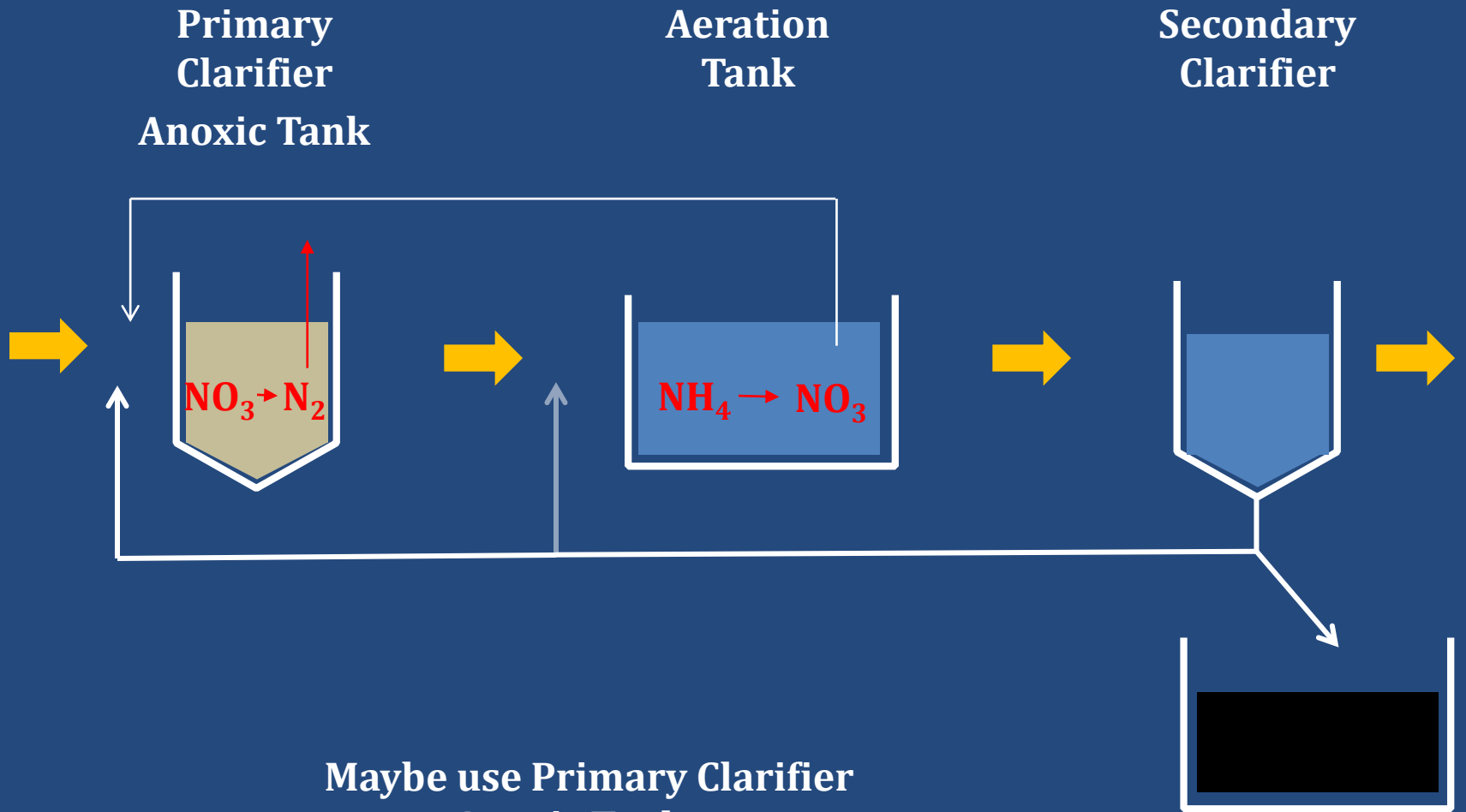
### Nitrate ( $\text{NO}_3$ ) Removal

Target:  $\text{NO}_3 < 4 \text{ mg/L}$   
ORP: -100 mV  
Unless RAS can be increased to 200% or more,  $\text{NO}_3$  target of 4 mg/L will be hard to achieve

### Sludge Holding Tank

*MLE Process Modification of Conventional AS Plant*





Maybe use Primary Clarifier  
as pre-Anoxic Tank

Maybe install Internal  
Recycle Pump(s)

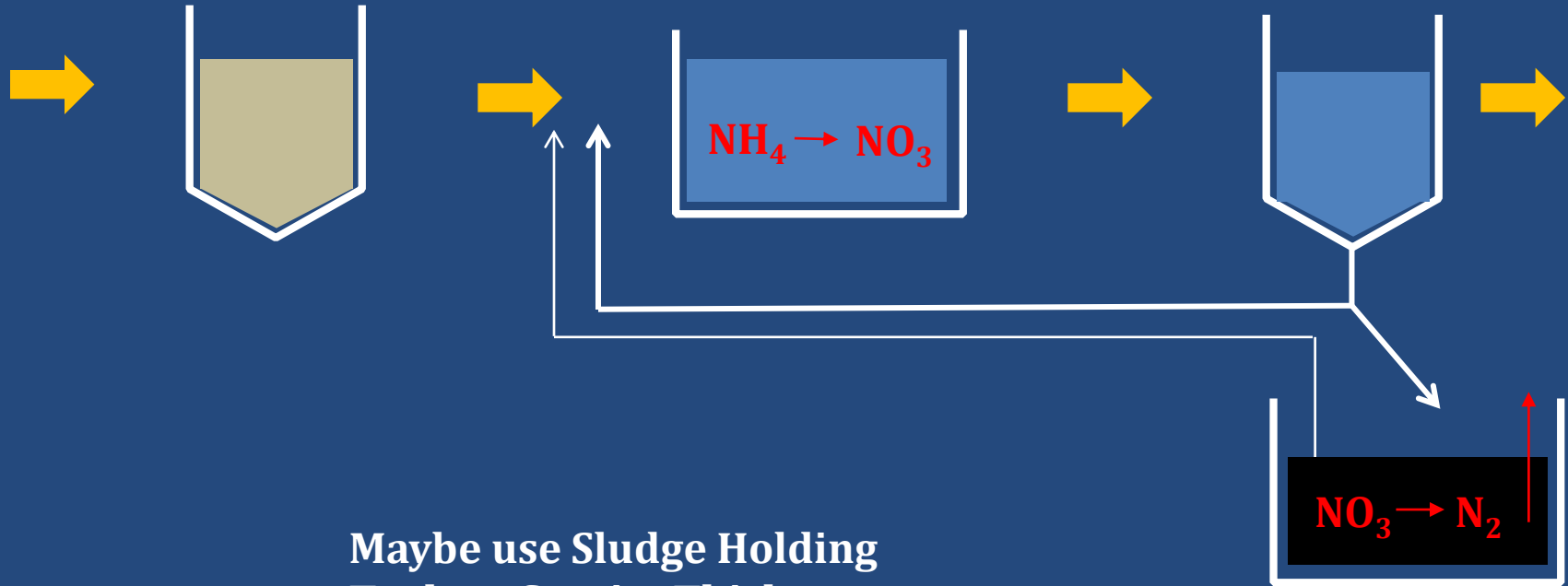
*MLE Process Modification of Conventional AS Plant*



Primary Clarifier

Aeration Tank

Secondary Clarifier



Maybe use Sludge Holding Tank or Gravity Thickener as post-Anoxic Tank

Sludge Holding Tank  
Anoxic Tank

*MLE Process Modification of Conventional AS Plant*

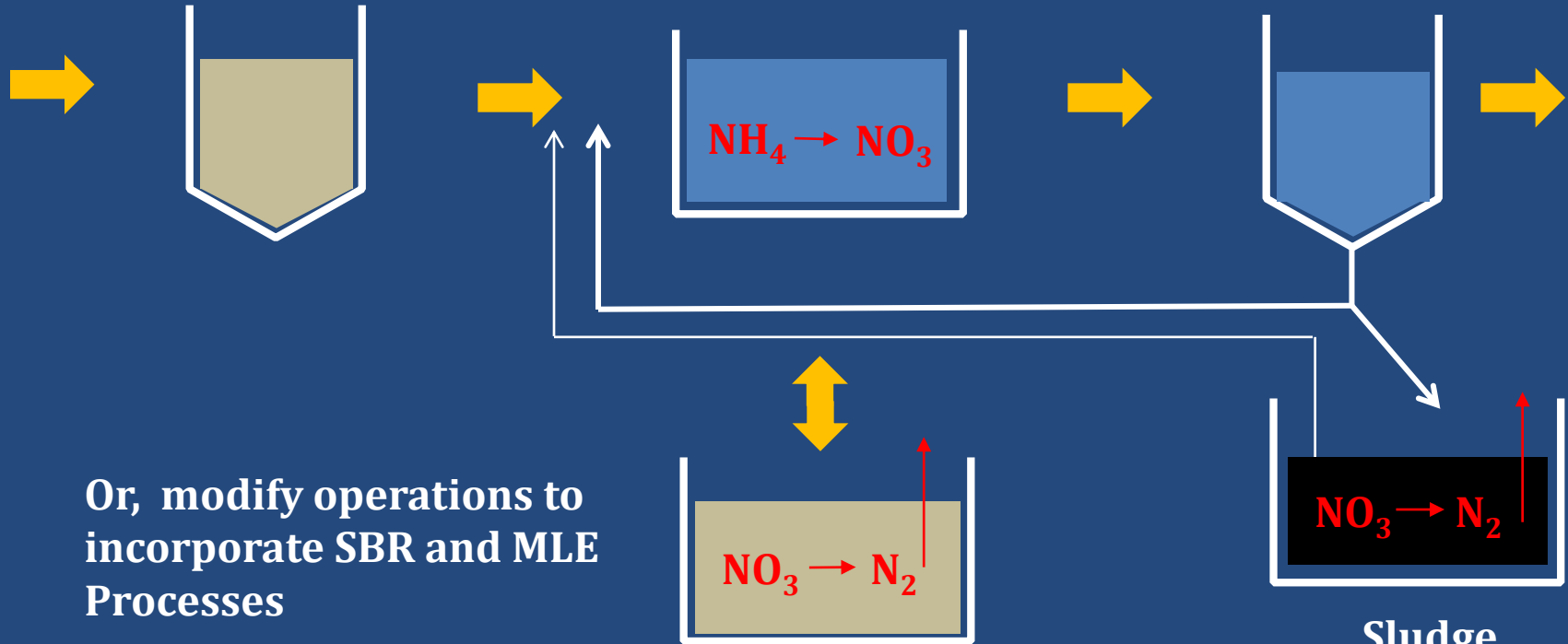




Primary Clarifier

Aeration Tank

Secondary Clarifier

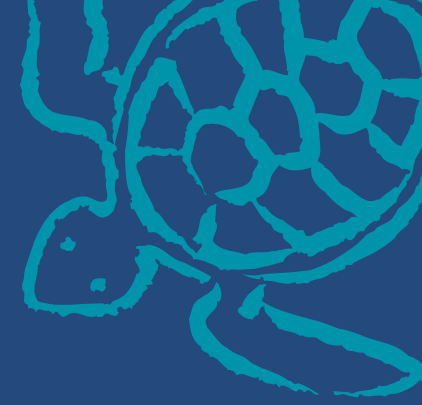


Or, modify operations to incorporate SBR and MLE Processes

Sludge Holding Tank  
Anoxic Tank

*MLE & SBR Modification of Conventional AS Plant*





## *Monitor and Control the Process*



Review and Analyze Data every day

Maintain Optimized Habitats

Monitor Treatment Efficiency

Be Prepared to make Process Changes every day

Preemptive changes to keep Habitats Ideal

Reactive changes to meet Treatment Requirements

# MONITORING NITROGEN



## Monitoring *HABITAT CONDITIONS*



Daily testing of ...

Process control parameters

SVI

MLSS

DO

ORP

Alkalinity



## *DO and ORP*



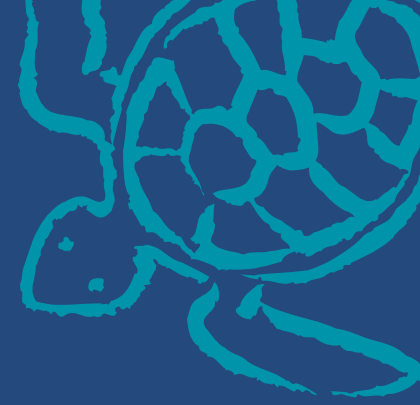
# Probes



## *Portable Analyzers*



## *pH and Alkalinity*





## Monitoring **TREATMENT**



# Monitoring Nitrogen



Daily testing of ...

Ammonia

Nitrate

Nitrite



## *Lab Spectrophotometer*



Daily testing of ...

Ammonia

Nitrate

Nitrite



# In-Line Nitrogen Probes



Ammonia  
Nitrate





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